Research Article



Preparation of cobalt ferrite nanoparticles using fulvic acid as a capping agent and its effect on catalytic activity

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Abstract:

Cobalt ferrite was prepared by co-precipitation from cobalt and iron soluble precursors in presence of fulvic acid at different pH values, namely, 6 and 8 and compared with the same preparation in absence of fulvic acid. The presence of fulvic acid is expected to bind metal ions through bridging before co-precipitation and mineralization. The extent of binding is determined according to the pH of the process. This influences the mineralization of the resulting cobalt ferrite and the crystallization/ordering of its lattice. In addition, the extent of residual ferric oxide is also a function of the efficiency of binding process. This route of modification for the co-precipitation process was found to be accompanied by enhanced surface area and total pore volume for most of the prepared samples. The involvement of these oxides as catalysts in the photo-catalytic degradation of phenol from wastewater was found to contribute very efficiently and the removal reached about 88% in some cases, which can be attributed to olation and oxolation process of the formed nanoparticles.

Keywords: nanostructured materials; precipitation; oxidation; X-ray diffraction

1. Introduction

The surface and catalytic activity of mixed metal oxides are mainly dominated by the methods of preparation and calcination conditions^[1-4]. Mixed oxides are mostly prepared to merge some properties that cannot be gained from single oxide. The development of new active compounds that can contribute to several fields of applications is a direct result for this merge of properties.

The very attractive properties of nanometric structures derived from metal oxides made them receiving great attention as promising materials for fields such as catalysis and adsorption ^[4-8]. Some reports in the open literature dealt with the adsorption of different dyes to surfaces such as iron oxides ^[9, 10].

Fabrication of adsorbents with controlled features like the size and crystallinity is a challenging task. Thus, the preparation procedure can have a major influence in terms of the chemical composition and microstructure. Co-precipitation is a facile method among those that have been employed for preparation of catalysts. It is favored because it leads to homogenous catalysts from the chemical point of view thereby both the surface and bulk of the prepared catalysts can contribute to catalytic course. These advantages made this method widely applicable to catalysts dedicated for performance under high pressure and moderate temperature [11-14]. As an example, the ferrites fabricated via the co-precipitation route acquired a non-aggregated and uniform structure [11-20]. Many studies explored the consequence of using some organic compounds on the coprecipitation process of metal ferrites ^[21-25]. Among them, polyvinyl pyrrolidone (PVP) was added as capping agent during the course of coprecipitation of cobalt ferrite [21]. Essawy and co-workers [26-28] used fulvic acid in the preparation of polymeric superabsorbents to pass on reinforcement and functionalization to the resulting structures. This provoked elevation of the chemical activity especially the chelation potential ^[26]. The high functionality and elevated binding capacity of fulvic acid to metal ions allowed their role as templates through the synthesis of metal oxides starting from nitrate precursors via coprecipitation ^[7,8]. This progresses via initial coprecipitation in the form of metal hydroxides in existence of fulvic acid and the

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desired oxides are finally obtainedby calcination at high temperatures. Grouping a number of precursors of metal ions in presence of fulvic acid would be expected to result in homogenous metal oxides exhibiting variation in their composition and characteristics ^[26-28].

Phenol is commonly used as a raw material for the preparation of many products. This includes pesticides, pharmaceutics, resins and many others. Nevertheless, it is toxic, carcinogenic, and non-biodegradable ^[29-32].

Pollution of water sources became a parallel fact to the numerous industrial activities. This necessitates the great need to take care of these pollutants prior to their transport into plants of wastewater treatment. Highly developed oxidation techniques are suggested deal with the organic contaminants present in water ^[33, 34]. Rigorous efforts are devoted to improve these technologies by changing the catalytic system or the oxidizing agent. Nevertheless, using catalysts that belong to oxidizing reagents in liquid phase may elevate this contamination.

The ongoing study is an effort to obtain nanometric mixed metal oxides incorporating iron and cobalt while revealing a wide range of surface characteristics and chemical composition following modified co-precipitation method of nitrate precursors in solution by employing sodium hydroxide in existence of fulvic acid at pH 6 and 8. This is expected to provide control over the rates of co-precipitation and hence changeable mineralization and ordering of the prepared mixed oxides. The use of such metal oxides as advanced oxidants in the solid form to stop any further contamination to the water through their catalytic cycle is also among the purposes of this study. The work will be also extended to their application in the photocatalytic removal of phenol from wastewater.

2. Experimental

2.1 Materials and methods

Fulvic acid was supplied from Changsha Xian Shan Yuan Agriculture Technology Co., China. Cobalt nitrate and ferric nitrate were purchased from Sigma-Aldrich, Germany. Phenol aqueous solution (80%, w/w) was obtained from BDH Chemicals, England. Otherwise, the rest were analytical grade chemicals that were used with no further purification.

2.2 Preparation of metal oxide nanoparticles via coprecipitation process

The wet chemical co-precipitation procedure was involved in the preparation of Cobalt ferrite $(\text{CoFe}_2\text{O}_4)^{[12]}$. Nitrates of cobalt and iron were dissolved in distilled water at a certain molar ratio (Fe/Co=2) while sodium hydroxide solution (1M) was used for the precipitation. The nitrate solutions and sodium hydroxide were mixed in existence of fulvic acid. The mixing was accomplished via drop wise addition from 3 different burettes into a collective vessel containing 1000 mL distilled water while continuous stirring was kept running. The dropping rate was managed in such a way to keep the pH (6 or 8) and the temperature (70 °C) unchanged during the co-precipitation. The precipitate was rinsed with distilled water several times to get rid of NO^{3-} and Na^+ ions. Filtration was undertaken followed by overnight drying at 100 °C. Lattice formation of the oxides was targeted by calcination at 700 °C for 4h. Thus, for simplicity, the sample prepared at pH 6 in absence of fulvic acid is denoted as P6 while F6 designates the same when fulvic acid was included in the recipe. Similarly, P8 reveals the coprecipitation performed at pH 8 in absence of fulvic acid whereas F8 indicates the equivalent sample prepared in existence of fulvic acid F8.

2.3 Measurements

X-ray diffractograms of the solids obtained by calcination at 700 °C were collected using Bruker diffractometer (D 8 advance target) with CuK_a secondly monochromator (λ = 1.5405 Å), operated at 40 kV and 40 mA, at a scanning rate of 0.8° 20 min⁻¹for phase identification and line broadening. The crystallite size of each phase calculated by Scherrer equation (Eq. 1):

$d = K \lambda / \beta_{1/2} \cos \theta$	((1))
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Where d represents the mean crystalline diameter, λ is the wavelength of x–rays, K is the Scherrer constant (0.89), $\beta_{1/2}$ is the full width at half maximum (FWHM) of the main peaks of diffraction and θ is the angle of diffraction.

The morphology and surface structure of the oxides were imaged by JEOL JEM-1230 transmission electron microscope (TEM) coupled with JEOL-SEM scanning electron microscope (SEM) operated at acceleration voltage of 80 kV.

The properties of the surface were investigated by undertaking adsorption of nitrogen gas at 350 °C using Quantochrome AS1WinTM- automated gas-sorption apparatus (USA). The samples were degassed at 200 °C for 2 h prior to the adsorption processes then the specific surface area (S_{BET}) was estimated by applying Brunauer–Emmett–Teller (BET) equation. On the hand, the pore size distribution was evaluated from the desorption part of the isotherm using the standard method.

The catalytic removal of phenol from wastewater was undertaken by suspending 1 g of mixed oxide in a glass reactor containing 100 mL of distilled water and 100 ppm of phenol and immersed in water bath fitted with temperature controller. Shaking on the solution was applied continuously at 150 rpm and 25 °C for up to 4 h.

For evaluation of the concentrations of residual phenol in wastewater, 5 mL suspension was withdrawn from the reactor and centrifuged for 10 min before recording the absorbance was performed at 270 nm using a calibrated UV-VIS spectrophotometer (UV-VIS-NIR-3101 PC, Shimadzu) ^[35]. The removal efficiency of phenol was assessed as average of three readings and applying Eq. 2:

Removal, $\% = ((A^{\circ} - A)) / (A^{\circ}) \ge 100$ (2)

Where A° and A are the absorbance of the blank and sample, respectively. According to Beer-Lambert's law, A° and A are proportional to C° and C, which refer to the concentrations of the blank and sample at time t $^{[35]}$.

3. Results and discussion

The X-ray diffractograms of mixed oxides prepared in presence and absence of fulvic acid before calcination at 700 °C are displayed in Figure 1 and summarized in Table 1.

Table 1. The effect of fulvic acid on the peak intensity of the main diffraction lines of Fe_2O_3 and CoFe_2O_4 along with their crystallite size .

Sample	Intensity (a.u.) of diffraction peaks for Fe_2O_3 and $CoFe_2O_4$		size of Fe ₂ O ₃ and CoFe ₂ O ₄ Crystallit (nm)	
	Fe ₂ O ₃	CoFe ₂ O ₄	Fe ₂ O ₃	CoFe ₂ O ₄
P6	130	106	93.3	72.8
P8	-	95.6	-	26.5
F6	-	66.8	-	23.4
F8	85.4	74.6	70.5	55.2

It is obvious from Figure 1 that the coprecipitation achieved at pH 6 in absence of fulvic acid (P6) took place with a portion of Fe_2O_3 not taking part in the reaction $(2\theta = 33^\circ)$ whereas cobalt ferrite $(2\theta = 35^\circ)$ was the major phase. When fulvic acid was involved in the process (F6), it propagated without formation of Fe_2O_3 while at pH 8, in absence of fulvic acid (P8), $CoFe_2O_4$, was born as a sole phase with high crystallinity (95.6 a.u.). Interestingly, at pH 8 the presence of fulvic acid (F8) led to birth of both Fe_2O_3 and $CoFe_2O_4$.

Table 1 signifies that the existence of fulvic acid at pH 8 (F8) gave rise to formation of nanometric Fe_2O_3 as a main component along with $CoFe_2O_4$ that underwent a two-fold increase in the crystallite size (55.2 nm) in comparison to the same procedure in absence of fulvic acid (26.5 nm, P8). The increase was accompanied by a visible decline in the crystallinity of $CoFe_2O_4$ (74.6 a.u.).



Figure 1.X-ray diffraction profiles for products of coprecipitations undertaken with and without fulvic acid after calcination at 700 °C; 1 indicates Fe_2O_3 , 2 indicates CoFe_2O_4 .

The observed significant high crystallite size of CoFe_2O_4 in case of F6 might have resulted from a considerable decline in the degree of dispersion of CoFe_2O_4 in its crystal lattice [1]. As so, CoFe_2O_4 is known with its catalytic activity while in this case the lack of distribution over its crystal lattice is expected to bring about a major drop in its catalytic activity, which was actually the case as will be shown in the next parts.

This could be better understood by the illustration presented in scheme 1 which shows that at pH 6, the fulvic acid present in a protonated form. Thus, the conditions are not appropriate for coordination of Fe³⁺ and Co²⁺ by fulvic acid. Opposite trend was encountered at pH 8 in which strong interaction developed between Fe3+ ions and the oxygenated and carboxylate sites. This suggests that this process might be dominated by the tendency of ferric hydroxide to precipitate first, which is harmonizing with the considerable variation in the solubility product values of the hydroxide precursors; 5.92×10^{-15} and 2.79×10^{-39} for cobalt and ferric ions, respectively. Accordingly, the fulvic acid is thought to have capped the ferric ions while another portion of ferric ions was involved in the construction of the uniformly distributed solid phase of cobalt ferriteas a result of calcination. During this process the organic material (fulvic acid) has been totally removed by calcination whereas Fe₂O₂ developed progressively phase. From Table 1, we can notice that particle size of Fe₂O₂ increases by the presence of fulvic acid. This may be ascribed to many close particles combine together and contribute to the particle size increase by melting of their surfaces [36].



Scheme 1. A suggested mechanism of involving interactions between fulvic acid and ferric ions at pH 6 and 8 prior to calcinations.

These findings were supported from high resolution transmission electron microscopy images (Figure 2 a-d). Figure 2a indicates the presence of two different groups of particles; one exhibits a size of 69-85 nm while the other one acquired a size between 22-28 nm. The inset of this image confirms that the heterogeneity of the electron diffraction is high which indicates incomplete mineralization of $CoFe_2O_4$ (XRD of P6, Figure 1). On the other hand, Figure 2 c ensures that the presence of fulvic acid (F6) caused drop in the overall crystallinity of the formed $CoFe_2O_4$ despite the complete coprecipitation reaction which leads to effective mineralization. Further, the electron diffraction shows no obvious change in the heterogeneity feature (inset of Figure 2 c).

Figure 2 b, d gives rise to the interesting feature

induced by existence of fulvic acid in the coprecipitation course whereupon the overall ordering became more homogenous (inset of Figure 2d) as compared to the same product in absence of the fulvic acid (inset of Figure 2b). In addition all the formed crystals were in the nanometric scale.

Therefore, it is noticeable that the size of crystallites and of crystallinity degree are very much dependent on the pH of the medium during precipitation and the presence a capping agent such as fulvic acid. This is in full accordance with earlier studies, which showed that fulvic acid can be involved in different ways during the coprecipitation due to its variable binding potential to metal ions at different pH values ^[35, 37].



Figure 2. High resolution transmission electron microscopy (HRTEM) imaging of , a: P6, b: P8, c: F6 and d: F8 after calcination at 700 °C.

Sample	$S_{_{BET}} \left(m^2/g \right)$	total pore volume Vp (cc/g)	mean pore radius r ⁻ (nm)
P6	7.3	0.06	164.4
P8	20.7	0.03	29.0
F6	11.4	0.01	17.5
F8	13.9	0.02	28.8

Table 2. Surface properties of the solids emerged from the various recipes after calcination at 700 °C.

Investigation of the surface properties for the prepared solids were accomplished by nitrogen gas adsorption-desorption as clear from Figure 3 and Table 2. It can be easily recognized that the involvement of fulvic acid at pH 6 (F6) caused a substantial increase in S_{BET} (56%) as compared to P6. This can be accounted for by the associated drop in r

(Table 2). On the other hand, the practical decrease of S_{BET} in existence of fulvic at pH 8 (F8) in comparison with P8, in which the fulvic acid was absent, can be justified by the domination of the increase in the crystallite size of $CoFe_2O_4$ (Table 1)



Figure 3. Corresponding nitrogen gas adsorption-desorption isotherms for the solids obtained bycalcination at 700 °C; a:P6, b: P8, c:F6 and d: F8.

This was motivating for us to carry out a preliminary photocatalytic study and employ the prepared metal oxides as catalysts during the photocatalytic degradation of phenol present in wastewater. Fig. 4 demonstrates an interesting catalytic action that increases progressively with the time and reaches 88% and 75% after 3h in case of F8 and P6, respectively. The catalytic efficiency can be arranged in the following order: F8>P6>P8>F6. The elevated catalytic activity of F8 and P6 with respect to the other formulations (P8 and F6) can be explained by a joint catalytic action of $CoFe_2O_4$ and Fe_2O_3 , which was not the case for P8 and F6. This may refer to enhancement of the catalytic power of $CoFe_{2}O_{4}$ by $Fe_{2}O_{3}$. This behavior might be attributed to olation of both metal ions in the form of hydroxides that could be survived during the calcination process. The olation-based structure exhibited oxolation during their employment in photocatalytic reactions which provides hydrogen ions that are able to combine with the phenol and causes its degradable as shown in scheme 2 [38-41].

$$\begin{split} [M(H_2O)_5OH]^{2+} + [M(H_2O)_6]^{3+} \rightleftharpoons & \{M(H_2O)_5(\mu\text{-}OH)M(H_2O)_5\}^{5+} + H_2O \\ & \{[M(H_2O)_5]_2(\mu\text{-}OH)\}^{5+} \rightleftharpoons \{[M(H_2O)_5]_2(\mu\text{-}O)\}^{4+} + H^+ \end{split}$$

Scheme 2. Chemical reactions illustrating the formation of olation-oxolation structure.



Figure 4. Photocatalytic removal efficiency of phenol using metal oxides prepared by calcination at 700°C.

4. Conclusions

Highly ordered cobalt ferrite can be prepared by modified coprecipitation process starting from cobalt nitrate and ferric nitrate in existence of fulvic acid at different pH values. Fulvic acid exhibits high coordination potential to the starting metal ions during the co-precipitation process. This provides control over the extent of mineralization and the crystallization/ordering of the resulting cobalt ferrite lattice. The control over the co-precipitation can contribute efficiently to the surface area and porosity which made these mixed oxides liable for catalytic applications. The use of the different forms of these oxides as catalysts in the photocatalytic degradation of phenol present in wastewater gives pronouncing levels of removal which reached 88%. This can be accounted for by enhancement of the photocatalytic activity as a result of combination of cobalt ferrite and ferric oxide in a structure exhibiting olation and oxolation.

Author Contributions: Jinxing LI and Dr. Abdelrahman A. Badawy as first author contributed equally to this work, finalize the experiment and gave the ideas. Prof. Xiaojian Zhou and Prof. Hisham A. Essawy, both are the responding author, responsible for whole manuscript.

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